

Effect of Supercritical Ethanol Drying on the Properties of Zinc Oxide Nanoparticles

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The synthesis, characterization, and application as polymers and anti-wear additives of nanosized zinc oxide particles obtained by conventional and supercritical ethanol drying are reported in this study. The nanoparticles of ZnO produced by the two different drying techniques were characterized using Fourier Transform Infrared (FT-IR) spectrophotometry, Scanning Electron Microscopy (SEM), X-ray Diffraction (XRD) and Thermogravimetric analysis (TGA) to elucidate the shape, size, composition, and stability of the nanoparticles. ZnO nanoparticles were then applied to poly (vinyl chloride) (PVC) powder and light mineral oil to assess their effectiveness and suitability as additives in diverse areas. XRD analysis revealed ZnO crystalline structure with average particle size of 24.7 nm for zinc oxide nanoparticles prepared by supercritical ethanol drying while SEM showed well-isolated and monodisperse particles with average size of 61.08 nm.

Keywords Mineral oil; Poly (vinyl chloride); Supercritical ethanol drying; Zinc oxide nanoparticles

INTRODUCTION

Nanoparticles are of considerable importance in numerous technological applications. The development of advanced functional nanomaterials for various applications, including catalysis, pigments, cosmetic sunscreens, textile materials, etc.,^[1–4] have received considerable interest in the last few years. Nanomaterials possess useful properties ranging from novel optical, electronic, and chemical properties^[5,6] to sunscreens, paints, varnishes, plastics, cosmetics,^[7] and lubricants.^[8]

Zinc oxide (ZnO) is an important material used for a variety of applications such as chemical sensors, varistors, thin-film luminescent devices, catalysts, and cosmetic materials.^[9] Due to the diverse applications of ZnO, the generation of highly dispersible materials homogeneously distributed in applied systems is of great importance as materials having a structure with a grain size in the nanometer range exhibit properties significantly different from

those for the same material with larger grain size. Ultrafine zinc oxide particles show a high degree of transparency, making them useful, especially for broad UV-A and UV-B blocking.^[7]

During production, nanoparticles agglomerate owing to the influence of interfacial tension during conventional drying.^[9,10] In order to prevent particle agglomeration during production, a number of new synthetic strategies have been developed to generate well-defined nanoparticles having structures and properties suitable for applications in aqueous and non-aqueous systems. Various methods for the preparation of metal oxide nanoparticles have been developed with the ultimate goal to produce particles of controllable properties including size distribution, morphology, and crystal structure. Amongst these methods is supercritical fluid drying, where the solvent is removed above its critical temperature (T_c) and critical pressure (P_c). High temperatures have been shown to be necessary in obtaining very fine particles as the liquid-vapor interface and capillary pressure are eliminated and the resulting particles do not tend to stick to each other.^[7,11–13]

The unique properties of supercritical fluids, mainly water, carbon dioxide, organic solvents, usually alcohols, have been demonstrated as a route for the production of metal oxide particles as they allow controlled particle properties, such as morphology, structure, and particle size distribution.^[14] Ethanol is a green fuel of the future, which can be regenerated from biomass through photosynthesis; therefore, ethanol can be used as a renewable bio-fuel. Ethanol has been used as an effective polar modifier for water and carbon dioxide in the supercritical fluid extraction and in supercritical chromatography.^[15]

The synthesis of zinc oxide (ZnO) nanoparticles using various methods has been reported in the literature.^[16–21] The use of supercritical fluid drying of ZnO has been investigated previously. Han et al.^[22] prepared ZnO nanoparticles in supercritical methanol and supercritical water and obtained particles down to 10 nm size. Gao et al.^[23] dried alcoholic ZnO gels by supercritical carbon dioxide drying. Monolithic zinc oxide aerogels were prepared

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using supercritical carbon dioxide by Krumm et al.^[24] Optical absorption and emission profiles and photocatalytic properties of ZnO nanoparticles were enhanced by supercritical fluid drying.

The introduction of nanoparticles into various systems has been shown to improve the properties of the system. For example, the dispersion stability of nano-sized particles in base oil provides the system to be used as a lubricant.^[25] When 0.5–3% nano ZnO was added to polyalphaolefin and surfactant solutions, the wear scar diameters were not lowered compared to the control mixtures without ZnO.^[26] This was attributed to insufficient dispersion of nano ZnO particles by the surface active agents added to polyalphaolefin. The introduction of nano-ZnO into polymer networks, e.g., PVC, has been reported^[27] to improve the structural, mechanical, and thermal properties of pure PVC. However, the effect of nano ZnO on the thermal stability of PVC was not reported previously.

There are many studies made with CO₂,^[22] water,^[21] and methanol^[20] in supercritical drying of ZnO. However, ethanol, which is a cheap and abundant solvent with lower critical pressure than other solvents such as CO₂, water, and methanol, has not been used for supercritical drying of ZnO. Thus, the preparation of zinc oxide nanoparticles by precipitation method and drying of the ethanol washed precipitates by conventional and supercritical ethanol drying were targeted in the present study. Removal of water and ethanol under supercritical conditions were made in order to prevent agglomeration of particles due to surface tension of liquid ethanol. The prepared zinc oxide nanoparticles were compared in properties by characterizing with SEM, X-ray diffraction, FTIR, and TGA. Their effects on PVC dehydrochlorination were investigated. Their dispersions in base oil were also tested as lubricants.

MATERIALS AND METHODS

Materials

Zinc chloride (ZnCl₂) from Fluka, sodium hydroxide (NaOH) from Merck, and ethanol (99.9% purity) from Merck were used as received in preparing zinc oxide (ZnO). All materials were used without further purification.

Preparation of ZnO Nanoparticles

Zinc oxide nanoparticles were prepared by the method developed by Belcheri et al.^[2] In a typical procedure, 11.0 g of ZnCl₂ was dissolved in 400 cm³ of ultrapurified water at 50°C in a water bath. 32 cm³ of 5 mol dm⁻³ NaOH aqueous solution was added “dropwise” to the zinc chloride solution with gentle stirring (125 rpm) over a period of 10 minutes at 50°C in a water bath. The particles were then separated from the supernatant dispersion by sedimentation and the resulting suspension washed firstly with

ultrapurified water, centrifuged at 6,000 rpm for 15 minutes, and secondly with ethanol and centrifuged also at 6,000 rpm for 15 minutes. The wet solid was divided into two portions. The first portion was left to dry at room temperature overnight and then placed in an air-circulating oven at 110°C until a constant weight was obtained after 3 hours (ZnO-A).

The second portion was dried at 250°C and 7.2 MPa above the critical conditions of ethyl alcohol (EtOH). The experiment was carried out using the supercritical extractor system as shown schematically in Figure 1. The system has a temperature-controlled 300 cm³ PARR 4561 (PARR Instrument Company, Illinois, USA) reactor (A) and a 300 cm³ PARR collector (B). Both reactors had 5.8 cm inner diameter and 10.1 cm height. Thus, the net volume is 272 cm³. The temperature controller had the following properties: “Model: PARR 4836, Input Thermocouple Type: J, Operating Range: 0–800°C, Readout Resolution: 1°C, Set point Resolution: 1°C, System Accuracy: ±2°C, Control Type: PID controller.” The pressure of the reactor (A) was monitored with a T316 stainless-steel Bourdon tube, with 7 × 10⁻³–20.9 MPa range having ±1% system accuracy. The reactor is equipped with a cooling coil to be used in cooling the contents further after the temperature dropped below the boiling point of the solvent in the reactor.

Before heating the system, nitrogen gas is passed through the system to remove oxygen in the reactor and pipelines. The critical temperature and pressure of ethanol are 239.8°C and 6.14 MPa. The supercritical drying was made under supercritical conditions of 7.2 MPa and 250°C. In a typical experiment, 5.05 g of wet solid and 100 cm³ ethanol were placed in the 300 cm³ reactor (A) (PARR 5500 Series Compact Reactor) and then the system was flushed with nitrogen gas. After all the valves are closed, the reactor A was heated up to 250°C.

When the temperature was 250°C and the pressure 7.2 MPa, the valve between the high pressure reactor and collector was opened to release ethanol into the 300 cm³

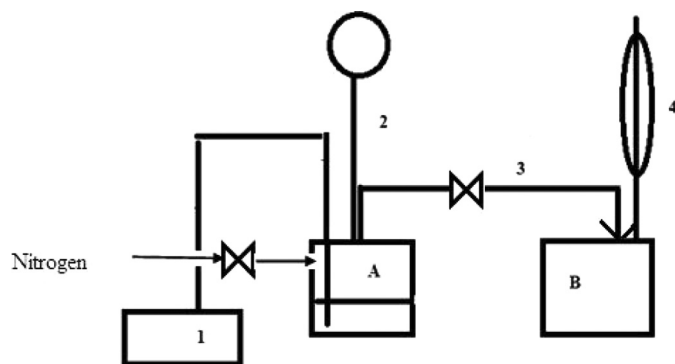
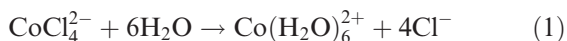


FIG. 1. Schematic representation of the supercritical drying system.

collector (B) at room temperature. The valve was closed after the pressure decreased to nearly zero. The reactor system is allowed to cool to room temperature. Ethanol mixed with water is condensed in reactor B.

Analysis of Ethanol Phase

The volume % water present in the ethanol phase after supercritical drying was measured using a simple analytical method based on the conversion of the blue CoCl_4^{2-} to pink $\text{Co}(\text{H}_2\text{O})_6^{2+}$ by addition of water.



The blue color of the ethanol solutions having 20 mg $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}/100 \text{ cm}^3$ ethanol and 0.5–2.0 $\text{cm}^3 \text{ H}_2\text{O}/100 \text{ cm}^3$ ethanol was measured as the absorbance at 670 nm using a Perkin Elmer (Massachusetts, USA) Lambda 45 UV/VIS spectrophotometer. A calibration curve of absorbance versus water concentration was drawn.

The water present in ethanol after supercritical drying was determined by adding 20 mg $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ to 100 cm^3 sample and measuring the absorbance at 670 nm. From the calibration curve, the water concentration was found.

Characterization of ZnO Nanoparticles

ZnO nanoparticles were prepared and dried by two methods: conventional (ZnO-A) and supercritical ethanol drying (ZnO-B) were characterized by various analytical methods. XRD was performed using an X-ray diffractometer (Philips Xpert-Pro from Panalytical, Almelo, Netherlands). The incident $\text{CuK}\alpha$ radiation at 45 kV and 40 mA with 1.54 Å was used in the analysis. The scattering data were collected in the 5–70° 2θ range. The dried sample powders were prepared in a 0.5-mm-thick holder. Fourier transform-infrared spectrophotometry (FT-IR) analysis was performed using a Shimadzu FTIR 8300S spectrophotometer from Shimadzu Kyoto, Japan. FT-IR was used to characterize the functional groups of the prepared nano-ZnO particles. FT-IR spectra of the samples were obtained in the spectral range 4000–400 cm^{-1} . Shimadzu TGA-51 was used for the thermogravimetric analysis of the samples. A small amount (10–15 mg) of each sample was taken for the analysis and the samples were heated from room temperature up to 600°C at 10°C min^{-1} under N_2 flow of 40 mL min^{-1} . SEM (Philips XL30 SFEG, FEI Company, Oregon, USA) images were used to observe the morphology of the samples. Conductive double-sided tape was used to fix the particles to the specimen holder before sputtering them with a thin layer of gold. The Zn, O, and Cl content of the ZnO nanoparticles were determined using elemental analyzer (Leco CHNS-932, Leco, Michigan, USA). Particle sizes of zinc oxide nanoparticles were determined using particle size analyzer Zetasizer 3000 HSA.

While using the zetasizer, the samples were dispersed in water by sonication.

Properties of Zinc Oxide Nanoparticles

ZnO Nanoparticles as Polymer Additive

The prepared samples were used as a polymer additive. PVC powder (1 g) and 0.1 g of the nano zinc oxide sample were blended thoroughly using an agate mortar and pestle. 0.5 g of this mixture was used to study the HCl evolution using conductivity measurements. Dehydrochlorination studies were carried out at 160 and 180°C using a Metrohm 763 PVC Thermomat (from Metrohm, Herisau, Switzerland) according to ISO 182-3. Metrohm 763 PVC Thermomat detects the evolution of HCl formed from the dehydrochlorination of PVC. The conductivity of the water solution to which the evolved HCl gas is transferred by carrier nitrogen gas versus time was measured and recorded. The measuring arrangement and experimental procedure of the Thermomat have been previously published.^[28]

ZnO Nanoparticles as Anti-wear Additive in Oil Lubricants

The tribological property of ZnO nanoparticles in a mineral oil was studied. In a typical experiment, 50 cm^3 of light mineral oil (TÜPRAŞ A.Ş.), 0.5 g of sorbitan monostearate (Span 60, Sigma-Aldrich) and 0.5 g of nano-sized ZnO powder were mixed thoroughly at 160°C for one hour on a magnetic hot plate and left to cool at room temperature. Four ball tests were done to determine the friction coefficient and wear scar diameter using a Four Ball Tester from FALEX Corporation, Illinois, USA. The test was performed according to ASTM D 4172-94 at 392 N and the test duration was 1 h.

RESULTS AND DISCUSSION

There are two opposing effects in supercritical drying of nanoparticles of ZnO: It may yield either nanoparticles of ZnO, since there is no surface tension to agglomerate the particles during drying, or monolithic ZnO particles form due to the reinforcing effect of high pressure on the walls of macropores of ZnO hydrogels.^[23]

Supercritical Ethanol Extraction

The amount of ethanol necessary to create the critical conditions in the reactor was calculated from the critical volume of ethanol (0.2756 g cm^3)^[27] and the reactor volume. Since the cooling coil and thermocouple insert in the reactor also occupied nearly 10 cm^3 , the volume of the reactor was taken as 260 cm^3 and 91 cm^3 liquid ethanol was required to create the critical conditions. Thus, an excess of this volume, 100 cm^3 ethanol, was added to the reactor to create supercritical conditions.

The change of pressure and temperature during the heating process of the reactor is shown in Figure 2a and Figure 2b, respectively. The reactor contents reached supercritical conditions (250°C and 7.2 MPa) in 50 minutes. The pressure-temperature diagram obtained during reaction is shown in Figure 2c. The measured change of pressure with temperature was very close to the predicted curve using the ancillary equation.^[29] In this ancillary equation, ethanol critical temperature (513.9 K) and pressure (6.148 MPa) were used as given below.

$$\ln \frac{P}{P_c} = \frac{T_c}{T} (-0.0514771\theta^{1/2} - 8.27075\theta - 5.49245\theta^3 + 5.64829\theta^{11/2}) \quad (2)$$

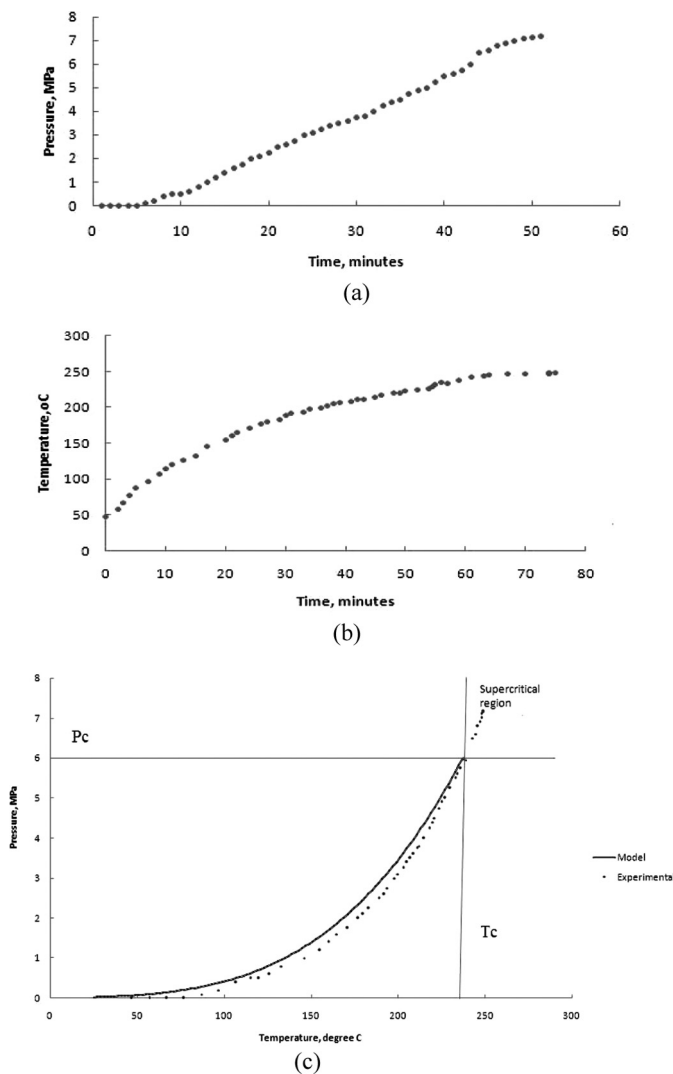


FIG. 2. (a) Pressure versus time; (b) Temperature versus time; (c) Pressure versus temperature during supercritical drying.

where $\theta = 1 - (T/T_c)$. It was noted that Equation (2) could be used to predict the vapor pressure of ethanol within $\pm 0.4\%$. The critical pressure and temperature obtained in the experiments was very close to the theoretical values.

The Material Balance

Water was removed from the samples in several steps. The first step is separation of the precipitated wet powders from aqueous solution by centrifugation. The second step is washing the precipitate with ethanol and separation of the powders from ethanol phase by centrifugation. Water in the samples was replaced with ethanol during washing of the sample with ethanol and centrifuging. When the samples were dried either by conventional drying or supercritical ethanol drying, the water and ethanol were removed from the system. 100 cm³ liquid ethanol was recovered in reactor B after the supercritical ethanol drying process. Some amount of ethanol (3–4 cm³) remained in pipes and could not be recovered. The ethanol vapor present at 250°C and 0.1 MPa in 300 cm³ reactor A was determined to be 0.31 g from an ideal gas equation. The ethanol remained in the reactor A after supercritical drying was not adsorbed by dried ZnO, since the FTIR and TG analysis indicated that ZnO (ZnO-B) collected in reactor A did not contain any ethanol. The water content of the recovered ethanol phase after supercritical drying process was determined as 0.32 cm³/100 cm³ ethanol (0.38% in mass). Thus, from 5.05 g of sample placed in the reactor, 0.32 g water and 4.73 g ethanol were separated by supercritical ethanol drying. The FTIR spectrum of the dried sample showed that there was only a small amount of water in the sample. Table 1 shows the compositions of the inlet and outlet streams of the reactor A.

The water present in the samples before supercritical ethanol drying was calculated as 6.4% since all water was removed by supercritical drying. All water and ethanol should have been removed from the samples at the end of either conventional drying or supercritical ethanol drying since the temperatures of conventional and supercritical drying processes were well above the boiling points of ethanol and water.

X-Ray Diffraction Measurements

The XRD patterns of ZnO nanoparticles are shown in Figures 3a and 3b, respectively. The X-ray diffraction exhibits the characteristic peaks for crystalline ZnO of hexagonal wurzite structure consistent with the standard values for ZnO.^[30] The sharp diffraction peaks indicate the good crystallinity of the prepared crystals. These peaks occurred at scattering angles (2θ) of 31.588, 34.228, 36.097° for ZnO-A, and 31.654, 34.328, 36.167° for ZnO-B. The high intensity peaks for ZnO-A and ZnO-B belonged to diffractions from (100), (002), and (101) planes of ZnO with JCPDS card number 79-0206.^[30] Although the peaks

TABLE 1
Composition of the streams in supercritical ethanol extraction assuming the solid phase is pure ZnO

Chemicals	Initial composition of the sample, mass %	Composition of the sample after supercritical ethanol drying, mass %	Composition of ethanol phase after supercritical ethanol extraction, mass %
ZnO	57.7	90	0
Ethanol	36.9	10	99.62
Water	6.4	0	0.38

occurring at 2θ values 11.1, 16.6, 22.0, 22.4, 24.7, 28.18 for both ZnO-A and ZnO-B samples is indicative of the presence of $\text{Zn}_5(\text{OH})_8\text{Cl}_2 \cdot \text{H}_2\text{O}$ with JCPDS card number 07-0155,^[31] it is more pronounced in the former. The peak at 2θ 11.1° belonged to (003) planes of $\text{Zn}_5(\text{OH})_8\text{Cl}_2 \cdot \text{H}_2\text{O}$. The relative intensities of this to 2θ 36.1° peak for ZnO-A and ZnO-B were 0.32 and 0.31, respectively. This indicated that ZnO-B had less $\text{Zn}_5(\text{OH})_8\text{Cl}_2 \cdot \text{H}_2\text{O}$ than ZnO-A, possibly due to its removal or partial transformation of $\text{Zn}_5(\text{OH})_8\text{Cl}_2 \cdot \text{H}_2\text{O}$ to other products during heating up to 250°C in the supercritical ethanol drying process.

The relative intensities of the peak at 2θ 34.2° of (002) planes to 2θ 36.1° peak of (101) planes for ZnO-A and

ZnO-B were 0.81 and 0.67, respectively. In bulk ZnO, this ratio is reported as 0.42 in JCPDS card number 79-0206. Both ZnO-A and ZnO-B particles were oriented in c-directions since this ratio was greater than 0.42. Supercritical ethanol drying process decreased the orientation in c-direction but crystals were still oriented in c-direction compared to bulk ZnO crystals.

The average particle size of the ZnO nanoparticles was calculated for three prominent peaks, (100), (002), and (101), using the Scherrer equation

$$L = \frac{K\lambda}{\beta \cos \theta} \quad (3)$$

where β is the measured full-width at half maximum (radians), θ is the Bragg peak angle of the peak, λ is the X-ray diffraction wavelength (in this case, it is 0.1546 nm), L is the effective particle size, and K is a constant = 0.9. The values are shown in Table 2.

The crystallite sizes 16.6, 16.7, and 16.8 nm estimated for (100), (002), and (101) diffraction lines were almost the same for ZnO-A. A higher crystallite, 27.7 nm, was obtained from (100) planes compared to sizes of 25.5 nm and 21.0 nm obtained from (002) and (101) planes for ZnO-B. The average particle size calculated using the Scherrer formula was 16.7 nm for ZnO-A and 24.7 nm for ZnO-B. The particles of ZnO increased in size by supercritical ethanol drying.

FTIR Spectrophotometric Analysis

Figure 4 shows the FTIR spectra of the synthesized ZnO nanoparticles.

The spectra clearly shows strong absorption bands at 407 cm^{-1} for ZnO-A and 420 cm^{-1} for ZnO-B associated

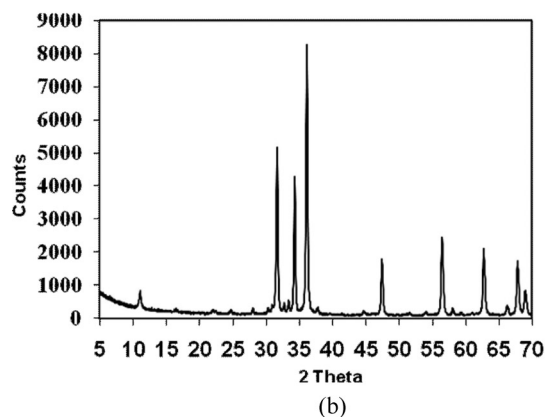
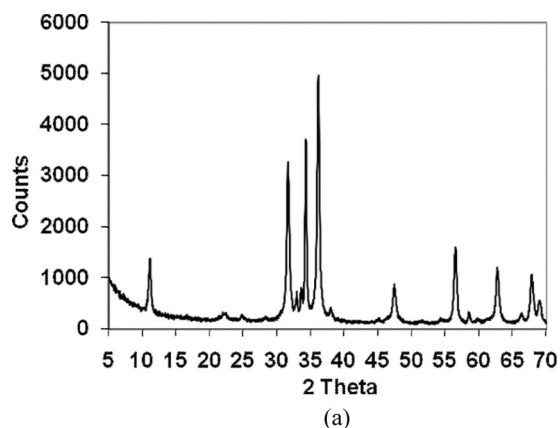


FIG. 3. XRD pattern for (a) nano ZnO-A; (b) nano ZnO-B.

TABLE 2
Crystallite sizes of ZnO nanoparticles

Sample name	Peak 1 (t_{100})	Peak 2 (t_{002})	Peak 3 (t_{101})	Average size
ZnO-A	16.6 nm	16.7 nm	16.8 nm	16.7 nm
ZnO-B	27.7 nm	25.5 nm	21.0 nm	24.7 nm

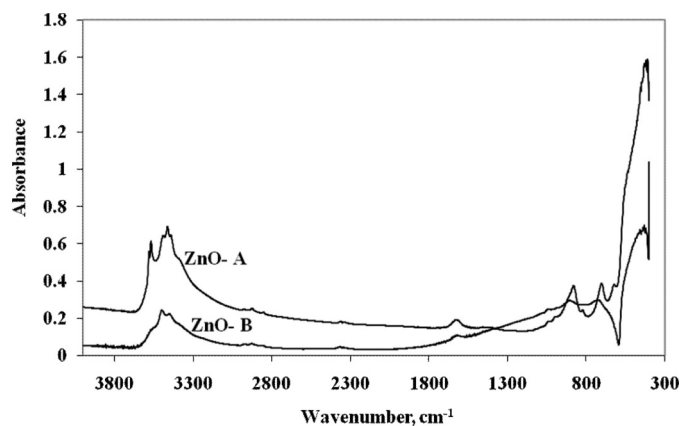


FIG. 4. FTIR spectra for synthesized ZnO nanoparticles.

with the characteristic vibrational mode of Zn-O bonding. The broad absorption peaks between 3450 and 3560 cm^{-1} for ZnO-A belonged OH stretching peaks of hydrogen bonded and isolated O-H groups. ZnO-B had only hydrogen bonded O-H groups vibrating at 3485 cm^{-1} for ZnO-B. There were no peaks in the region of 2900–2950 cm^{-1} related to symmetric and asymmetric stretching vibrations of CH_3 and CH_2 groups of ethanol in the spectra of both samples. This indicated that ZnO-A and ZnO-B were free of ethanol. Both samples had a very small amount of adsorbed water having bending vibration at 1600 cm^{-1} . The ratio of absorbance values at 3400 cm^{-1} for hydrogen bonded OH to 407 cm^{-1} for Zn-O was around 4 for both samples, indicating that they had nearly the same concentration of hydrogen bonded OH groups. The peak of isolated OH groups at 3566 cm^{-1} disappeared by supercritical ethanol drying process. The peaks at 713 and 893 cm^{-1} attributed to ZnO stretching vibrations^[32] were broadened in supercritical ethanol drying process.

Thermogravimetric Analysis

The thermal behavior of ZnO nanoparticles was studied using TGA. The TG curves are shown in Figures 5a and 5b.

There is an instrument drift of the TG analyzer starting from 30°C up to 160°C. The TG curves showed that there were no mass losses up to 160°C. If ethanol was present in the samples, it would evaporate at its boiling point of 78°C and step mass loss would be observed at this temperature. Thus, TG analysis also indicated that there was no ethanol in both ZnO-A and ZnO-B samples. There were two steps in mass loss during heating up to 600°C: 1.2% mass loss between 160–180°C and 2% between 375–400°C. From XRD measurements, $\text{Zn}_5(\text{OH})\text{Cl}_2 \cdot \text{H}_2\text{O}$ was present and with heat it decomposes finally, to form ZnO and H_2O as shown in Equations (4)–(6).^[32] Reactions 4 and 6 should have occurred during the supercritical ethanol drying

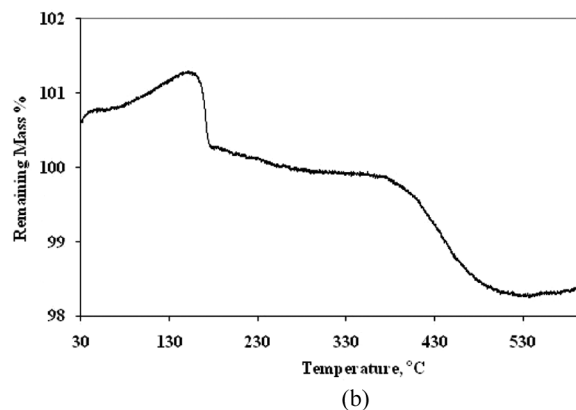
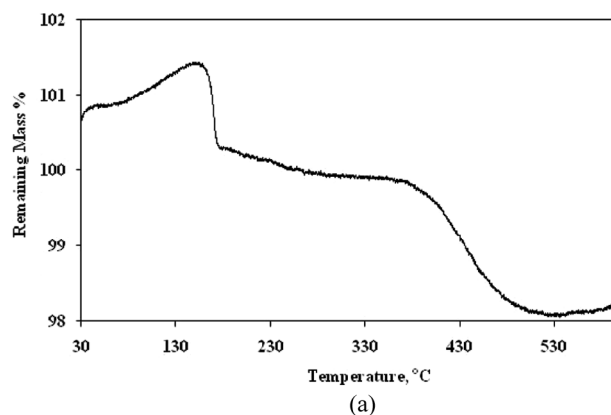
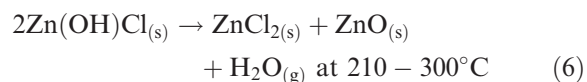
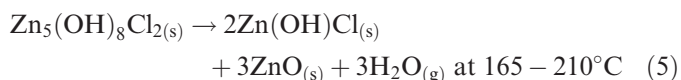
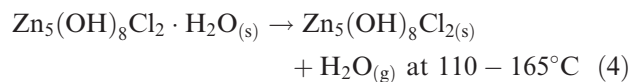


FIG. 5. TG curve for (a) nano ZnO-A; (b) nano ZnO-B.

process. However, both conventionally dried and supercritical ethanol dried samples had the same TG curves, indicating that the formed water was not separated from both samples during drying. Further heating in the TG analyzer allowed the evaporation of water in two steps starting at 160°C and 375°C.



The Morphology of ZnO Nanoparticles

Particle morphology and size were determined from scanning electron micrographs (SEM). Figures 6a and 6b show the micrographs of ZnO-A and ZnO-B nanoparticles at 200 and 500 nm scales.

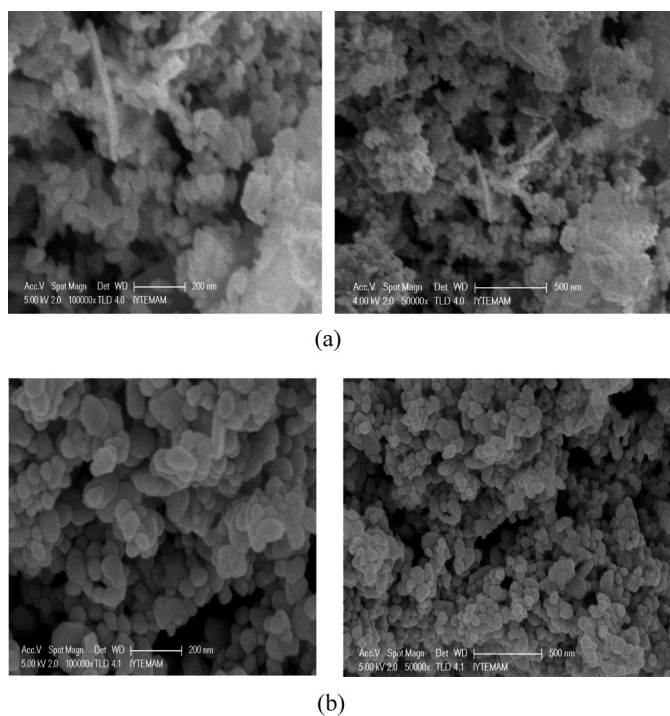


FIG. 6. SEM micrograph for (a) nano ZnO-A; (b) nano ZnO-B.

The SEM micrograph for ZnO-A presents aggregates made of spherical particles that are in the range of 50–100 nm with macropores between particles that have diameters larger than 50 nm. Nanoparticles are nearly spherical and quite monodisperse. However, there are some larger aggregates in the sample obtained from conventional drying. ZnO-B nanoparticles obtained after supercritical ethanol drying are flat particles, more monodisperse and isolated. The average sizes for the particles using SEM measurements were 53.47 and 61.08 nm for ZnO-A and ZnO-B, respectively. The crystal size of ZnO calculated from XRD data was smaller than that of the particles observed in SEM images. This indicates that the particles observed in SEM micrographs were agglomerated primary particles.

EDX Analysis of the Samples and Reactions Occurring during the Precipitation Process

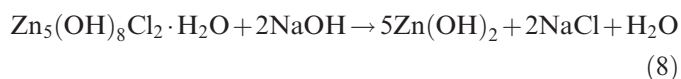
The approximate composition of the samples determined by EDX analysis is shown in Table 3.

The values obtained are average values selected from three randomly chosen points. The results indicate that ZnO nanoparticles contained >95% ZnO. However the Zn content was higher than expected for pure ZnO. The chlorine content, 3.2% of the supercritical ethanol dried sample ZnO-B, was lower than that of the conventionally dried sample, 5.3%. The lower chlorine content could be attributed to sublimation^[33] of ZnCl₂ formed according

TABLE 3
EDX analysis of ZnO nanoparticles

Sample	Zn (%)	O (%)	Cl (%)
ZnO-A	81.1	13.6	5.3
ZnO-B	83.7	12.8	3.2
Pure ZnO	76.4	24.4	0.0

to Equation (6). The EDX analysis of ZnO-A and ZnO-B samples indicated that during the precipitation reaction, pure ZnO was not formed, contrary to expectation.^[2] A small amount of Zn₅(OH)₈Cl₂·H₂O remained in ZnO. The consecutive reactions shown by Equations (7)–(9) are thought to occur during precipitation.



In the precipitation reaction, 1:2 molar ratio of Zn²⁺ and OH ions was used to ensure the formation of pure ZnO. However, since NaOH was added dropwise to ZnCl₂ solution initially, Zn₅(OH)₈Cl₂·H₂O was formed according to reaction 6 and some of it remained unchanged as X-ray diffraction studies revealed.

Particle Size Distribution

The particle size was determined by means of dynamic light scattering on a Zetasizer 3000 HSA. Figures 7a and 7b present size distributions (number average) of the ZnO nanoparticles.

The peak analyses obtained from the light scattering measurements are presented in Table 4.

Since ZnO particles were disc-shaped rather than spherical in shape, two consecutive runs of the particle size distribution in water were not identical but close to each other. The particles in water were more agglomerated in water than their dry state since higher average particle sizes were observed in Zetasizer than were observed in SEM pictures. 95% of the samples had 78.1 nm particle size in run 2 for ZnO-A and 92% of the samples had 107.7 nm average particle size for ZnO-B. Since the particles were flat in shape and the Zetasizer assumes spherical particles, it was not possible to obtain identical size distributions for the same sample in consecutive runs.

However, supercritically dried ZnO had larger particles than conventionally dried samples, indicating ZnO particles were agglomerated in the supercritical drying process due to applied high pressure. The effect of pressure

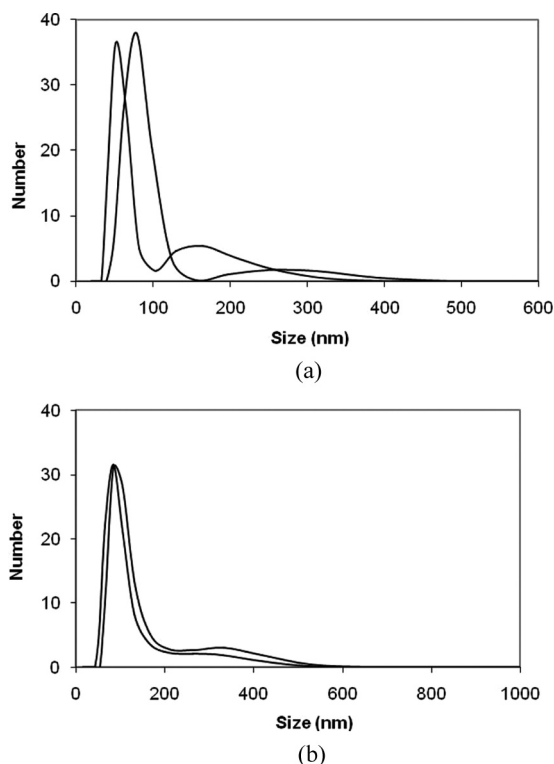


FIG. 7. Size distribution (number average) for (a) ZnO-A; (b) ZnO-B.

TABLE 4
Peak analysis for number average size distribution

	Peak	Area	Mean (nm)	Width
ZnO-A run 1	1	83.17	56.8	29
ZnO-A run 2	1	95	78.1	43.9
	2	5	268.7	174.5
ZnO-B run 1	1	100	104.4	55.2
ZnO-B run 2	1	92.3	107.7	55.2
	2	7.7	340.3	113.4

outweighs the absence of interfacial tension between the particles and the liquids that would keep the size of the initially formed nanoparticles constant without any agglomeration.

APPLICATION POTENTIAL OF ZnO NANOPARTICLES IN DIVERSE AREAS

Zinc Oxide Nanoparticles as Polymer Additive

Polymeric materials are of special interest because, in combination with suitable metal salts (lithium ions and/or ZnO), they give complexes that are useful for the development of advanced high-energy electrochemical devices, e.g., batteries, fuel cells, electrochemical display devices, and photoelectrochemical cells, with ease of fabrication into

thin films of desirable sizes.^[27] Poly (vinyl chloride) (PVC) is one of the major thermoplastics used today, having large and broad uses in commerce. It has the unique ability to be compounded with a wide variety of additives, making it possible to produce materials in a range from flexible elastomers to rigid compounds. One of the problems associated with the processing and use of PVC is its low thermal stability. Metal soaps from zinc salts have been shown to be effective thermal stabilizers for PVC.^[34-36]

The effect of the nanosized ZnO particles on the thermal stability of PVC powder was investigated using the 763 PVC Thermomat. The conductivity versus time curves obtained for the samples heated at 160 and 180°C are shown in Figures 8a and 8b, respectively.

Conductivity measurements provide an overall assessment of the relative effect of an additive on the process of dehydrochlorination of PVC. The induction time, stability time, and activation energies computed from values obtained from the induction times are presented in Table 5.

The induction time for pure PVC was 1.5 hr and 0.76 hr at 160°C and 180°C, respectively. For ZnO-A and ZnO-B samples added to PVC, the induction times at 160°C were

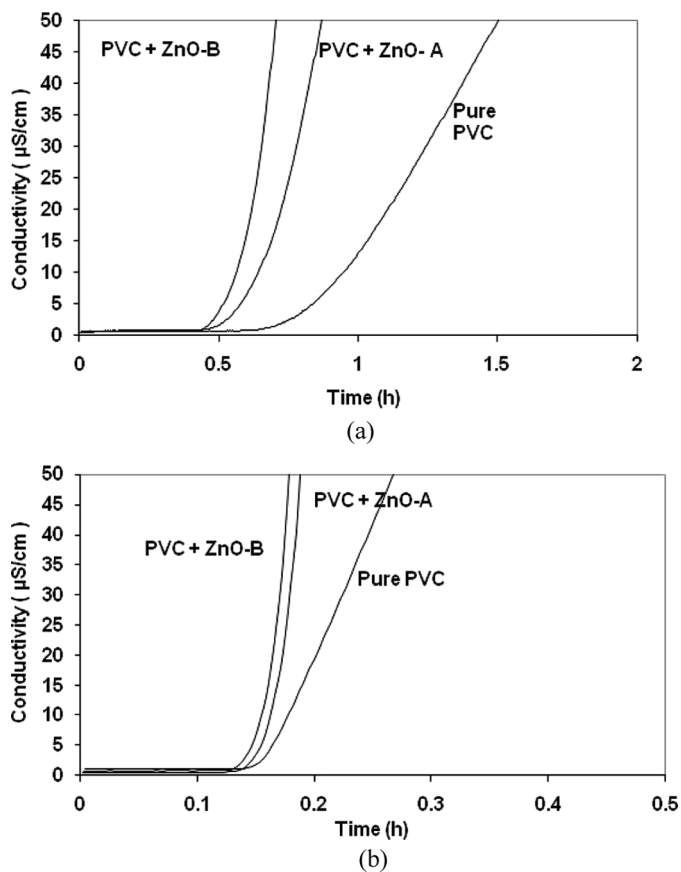


FIG. 8. Conductivity versus time curves for PVC and PVC having nanosized ZnO particles at (a) 160°C; (b) 180°C.

TABLE 5
Onset time, stability time, and activation energy of the stability time from conductivity measurement from PVC thermomat

Sample	Onset time, hr		Stability time, hr		Activation energy of the stability time, kJ/mol
	160°C	180°C	160°C	160°C	
PVC	0.76	0.09	1.50	0.25	141.2
PVC + ZnO-A	0.74	0.20	0.87	0.26	126.3
PVC + ZnO-B	0.71	0.18	0.73	0.19	116.3

not changed extensively compared to the control sample. The induction time increased from 0.09 hr to 0.20 and 0.18 hr by ZnO-A and ZnO-B addition, respectively, indicating the stabilizing action of both ZnO samples at this temperature. After onset of the dehydrochlorination, the added ZnO samples accelerated the dehydrochlorination reaction of PVC and the stability time at 160°C decreased from 1.5 hr to 0.87 and 0.73 hr for ZnO-A and ZnO-B, respectively. A similar behavior was observed at 180°C and stability time decreased from 0.25 hr to 0.19 and 0.18 hr for ZnO-A and ZnO-B addition.

It is expected that the addition of an additive to PVC should result in higher values of activation energy for the dehydrochlorination if it acts as a heat stabilizer. However, the addition of ZnO nanoparticles lowered the energy of activation from 141.2 kJ/mol to 126.3 and 116.3 kJ/mol for ZnO-A and ZnO-B, respectively. The activation energy of the control PVC sample was close to the values determined in previous studies.^[36] From the values, the addition of nanosized ZnO powder to PVC accelerated dehydrochlorination after onset of dehydrochlorination with more notable changes occurring in ZnO-B. The ZnO powders could be efficiently used in dehydrochlorination of waste PVC to obtain HCl.

ZnO Nanoparticles as Anti-wear Additive in Oil Lubricants

Numerous nanoparticles used as oil additives have been investigated in recent years and results show that they deposit on the rubbing surface and improve the tribological properties of the base oil, displaying good friction and wear reduction characteristics even at concentrations below 2 wt%.^[8] Commercially available lubricants contain base oil and functional additive packages to achieve a desired performance for a specific application. Antiwear additives are used to react with surfaces in contact to form a protective layer, which ensures that sporadic asperity contacts does not lead to severe wear.^[37] Nanoparticles of ZnO were used as a friction-reducing and antiwear additive for poly alpha olefin 6 in a previous study.^[8,26] In the present study, ZnO samples dried conventionally and by supercritical ethanol drying were used for the same purpose. The wear

scar surfaces of lower balls of the four ball tester are seen in Figure 9 for ZnO-A and ZnO-B added lubricants.

The wear scar diameter and friction coefficients of ZnO-A and ZnO-B added lubricants (Table 6) were smaller than paraffin oil but higher than the paraffin oil with Span 60. While ZnO-A had a lower friction coefficient (0.085) than ZnO-B (0.96), the wear scar diameter (0.079 mm) was lower for ZnO-B than for ZnO-A (1.145 mm). Thus, a compromise should be made to either lower friction coefficient or wear scar diameter by using two different ZnO samples. Battez et al.^[26] also observed an increase in wear scar diameter when nano ZnO was added to non-ionic surfactant added polyolefin oil. A similar behavior was observed in the present study for both ZnO-A and ZnO-B particles, indicating they were not dispersed in the oil. Even if they were softer than steel balls, when squeezed between

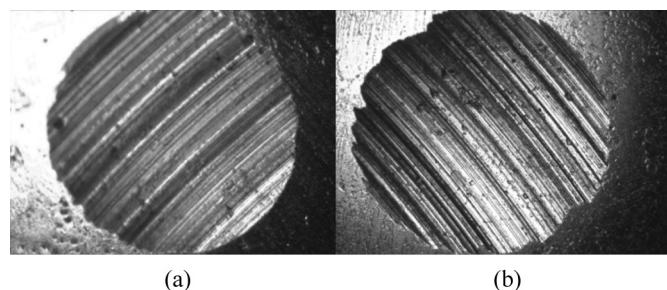


FIG. 9. Wear scar diameter of balls tested with using lubricant prepared from (a) ZnO-A; (b) ZnO-B.

TABLE 6
Friction coefficient and wear scar diameter of lubricants

Sample	Friction coefficient	Wear scar diameter, mm
Oil (Atakul et al., 2011)	0.099	1.402
Oil + Span 60 (Atakul et al., 2011)	0.064	0.639
Oil + Span 60 + ZnO-A	0.085	0.961
Oil + Span 60 + ZnO-B	0.079	1.145

the rotating upper ball and fixed lower balls they were hardened and eroded the steel surface.

CONCLUSIONS

ZnO nanoparticles were obtained by conventional and supercritical ethanol drying. The EDX analysis, X-ray diffraction, and TG analysis indicated that they contained small amounts of $Zn_5(OH)_8Cl_2 \cdot H_2O$, which decomposed partially during the supercritical ethanol drying process. The nanoparticles having 16.7 nm size were transformed to larger particles with 24.7 nm size by supercritical ethanol drying. The average sizes for the particles using SEM measurements were 53.47 and 61.08 nm for ZnO-A and ZnO-B, respectively. The particles were aggregated to larger particles, 78.1 nm and 107.7 nm sizes for ZnO-A and ZnO-B, respectively, in water. The absence of surface tension of liquid ethanol during supercritical ethanol drying was not sufficient to prevent agglomeration of the particles. Due to very high pressure used in supercritical extraction, the particles obtained were more agglomerated compared to the particles obtained by conventional drying at atmospheric pressure. The supercritically dried ZnO dehydrochlorinated PVC faster than conventionally dried ZnO. While a lubricant with ZnO-A had a lower friction coefficient than the lubricant with ZnO-B, the wear scar diameter was lower for ZnO-B than for ZnO-A. The supercritical ethanol drying of zinc oxide could be used for the purpose of obtaining more active PVC dehydrochlorination catalyst.

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